

HAYNES et al
Appl. No. 10/563,920
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AMENDMENTS TO THE CLAIMS:

This listing of claims will replace all prior versions, and listings, of claims in the application:

1-24 (cancelled).

25 (currently amended). A process for the production of acetic acid by reacting with carbon monoxide, methanol and/or a reactive derivative thereof in a liquid reaction composition comprising methyl acetate, a finite concentration of water, acetic acid and a catalyst system, which catalyst system comprises an iridium carbonylation catalyst, methyl iodide co-catalyst, at least one non-hydrohalogenoic acid promoter and optionally at least one of ruthenium, osmium, rhenium, zinc, gallium, tungsten, cadmium, mercury and indium and at least one non-hydrohalogenoic acid promoter.

26 (previously presented). A process according to claim 25 wherein the non-hydrohalogenoic acid is selected from an oxoacid, a superacid, a heteropolyacid and mixtures thereof.

27 (previously presented). A process according to claim 26 wherein the non-hydrohalogenoic acid is an oxoacid.

28 (previously presented). A process according to claim 27 wherein the oxoacid is an oxoacid of the elements of Groups 13 to 17 of the Periodic Table.

29 (previously presented). A process according to claim 27 wherein the oxoacid is selected from H₂SO₄, HNO₃, H₃PO₄ and mixtures thereof.

30 (currently amended). A process according to claim 27 wherein the molar ratio of oxoacid anion to iridium is in the range [greater than 0 to 0.4] : 1 greater than 0 to 0.4 : 1.

31 (currently amended). A process according to claim 29 wherein the molar ratio of oxoacid anion to iridium is [greater than 0 to 0.35] : 1 greater than 0 to 0.35 : 1.

32 (previously presented). A process according to claim 26 wherein the non-hydrohalogenoic acid is a superacid.

33 (previously presented). A process according to claim 32 wherein the superacid has a non-coordinating anion to iridium.

34 (previously presented). A process according to claim 32 wherein the superacid is a superacid having an anion selected from BF₄⁻, PF₆⁻, (CF₃SO₂)₂N⁻, CBH₆Br₆⁻, CF₃SO₃⁻, SbF₆⁻, FSO₃⁻ and mixtures thereof.

35 (previously presented). A process according to claim 32 wherein the superacid is selected from HBF₄, HPF₆, (CF₃SO₂)₂NH, HCBH₆Br₆ and mixtures thereof.

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36 (currently amended). A process according to claim 32 wherein the molar ratio of the superacid anion to iridium is in the range ~~[greater than 0 to 2.5] : 1 greater than 0 to 2.5 : 1.~~

37 (currently amended). A process according to claim 36 wherein the molar ratio of the superacid anion to iridium is in the range ~~[greater than 0 to 1] : 1 greater than 0 to 1 : 1.~~

38 (previously presented). A process according to claim 26 wherein the non-hydrohalogenoic acid is a heteropolyacid.

39 (currently amended). A process according to claim 38 wherein the heteropolyacid comprises at least one of molybdenum and/or tungsten as peripheral atoms.

40 (previously presented). A process according to claim 39 wherein the heteropolyacid is selected from 12-tungstophosphoric acid, 12-molybdophosphoric acid, 12-tungstosilicic acid, 12-molybdsilicic acid and mixtures thereof.

41 (currently amended). A process according to claim 38 wherein the molar ratio of the heteropolyacid anion to iridium is in the range ~~[greater than 0 to 5] : 1 greater than 0 to 5 : 1.~~

42 (currently amended). A process according to claim 41 wherein the molar ratio of the heteropolyacid anion to iridium is in the range ~~[greater than 1 to 4] : 1 greater than 1 to 4 : 1.~~

43 (previously presented). A process according to claim 25 wherein the catalyst comprises at least one of ruthenium, osmium, rhenium, zinc, gallium, tungsten, cadmium, mercury and indium.

44 (previously presented). A process according to claim 43 wherein the catalyst comprises at least one of ruthenium, osmium, rhenium and indium.

45 (canceled).

46 (previously presented). A process according to claim 25 wherein the concentration of methyl acetate in the liquid reaction composition is in the range 1 to 70% by weight.

47 (previously presented). A process according to claim 46 wherein the methyl acetate concentration is in the range 2 to 50% by weight.

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48 (previously presented). A process according to claim 25 wherein the concentration of water in the liquid reaction composition is in the range 1 to 15% by weight.

49 (previously presented). A process according to claim 48 wherein the concentration of water is in the range 1 to 10% by weight.

50 (previously presented). A process according to claim 25 wherein the process is carried out as a continuous process.